

REINHOLD ENVIRONMENTAL Ltd.



2015 Wastewater-Ash Round Table Presentation

September 22, 2015, in Charlotte, NC / Hosted by Duke Energy


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Physical/Chemical Treatment System Design Considerations

Ralph Cutler

2015


Factors Affecting Wastewater Characteristics

- Fuel type/Switching/Blending
 - Limestone Quality
 - Upstream Flue Gas Treatment
 - Scrubber Operation
 - Reagent Addition
 - Dewatering Options
- 

Factors Affecting FGD Wastewater Treatment Process Selection/Design

- pH
- Temperature
- Residence Time
- Solids Concentration
 - Feed
 - Reactor
 - Underflow

Factors Affecting FGD Wastewater Treatment Process Selection/Design

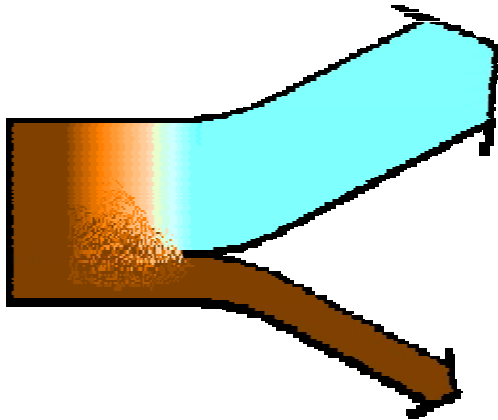
- Solids Particle Size Distribution
 - Constituent Concentration and Speciation
 - Plant Operation
 - Base Load
 - Peaking
 - Treatment Objectives- Treated Water Quality
 - Downstream Treatment
 - Disposal of Dewatered Solids
- 

Physical Unit Processes

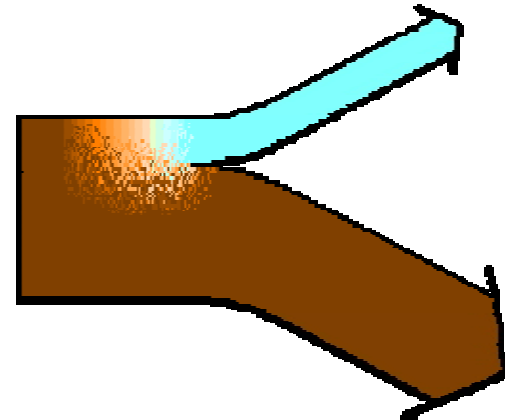
- Equalization
 - Tank
 - Mixed versus Un-mixed
 - Lined Basin
- Flocculation
- Sedimentation
 - Clarifier versus Thickener
- Gravity Sedimentation includes both Clarifiers and Thickeners

But – What's The Difference ?


Clarifiers =
Overflow



Thickeners =
Underflow



Physical Unit Processes

- Standard Clarifier
 - Flocculating Clarifier
 - Solids Contact Clarifier
 - Lamella Clarifier
 - Plates versus Tube Settlers
 - High Rate Clarification
 - Ballasted Flocculation/Sedimentation
 - Thickener
- 

Physical Unit Processes

- Clarifier Sizing Criteria

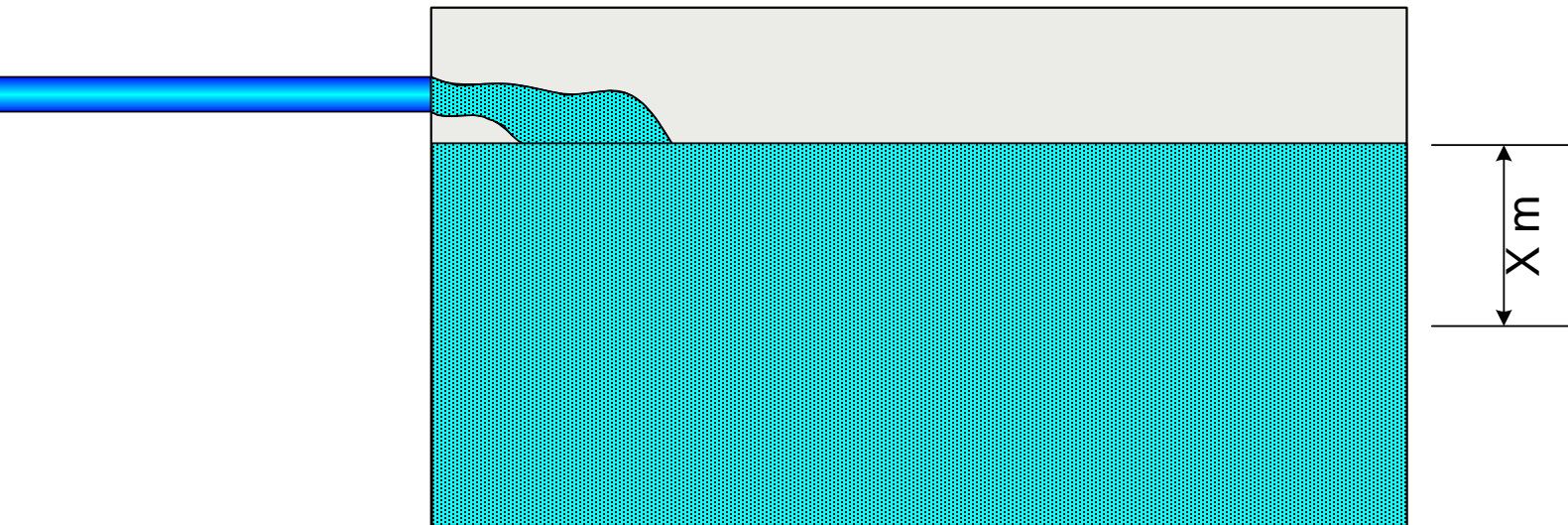
Clarifier Sizing

- The Minimum Diameter is Determined by:
 - Settling Rate/Rise Rate
 - Hydraulic loading
 - Unit Area Requirement
 - Solids loading

What is Rise Rate

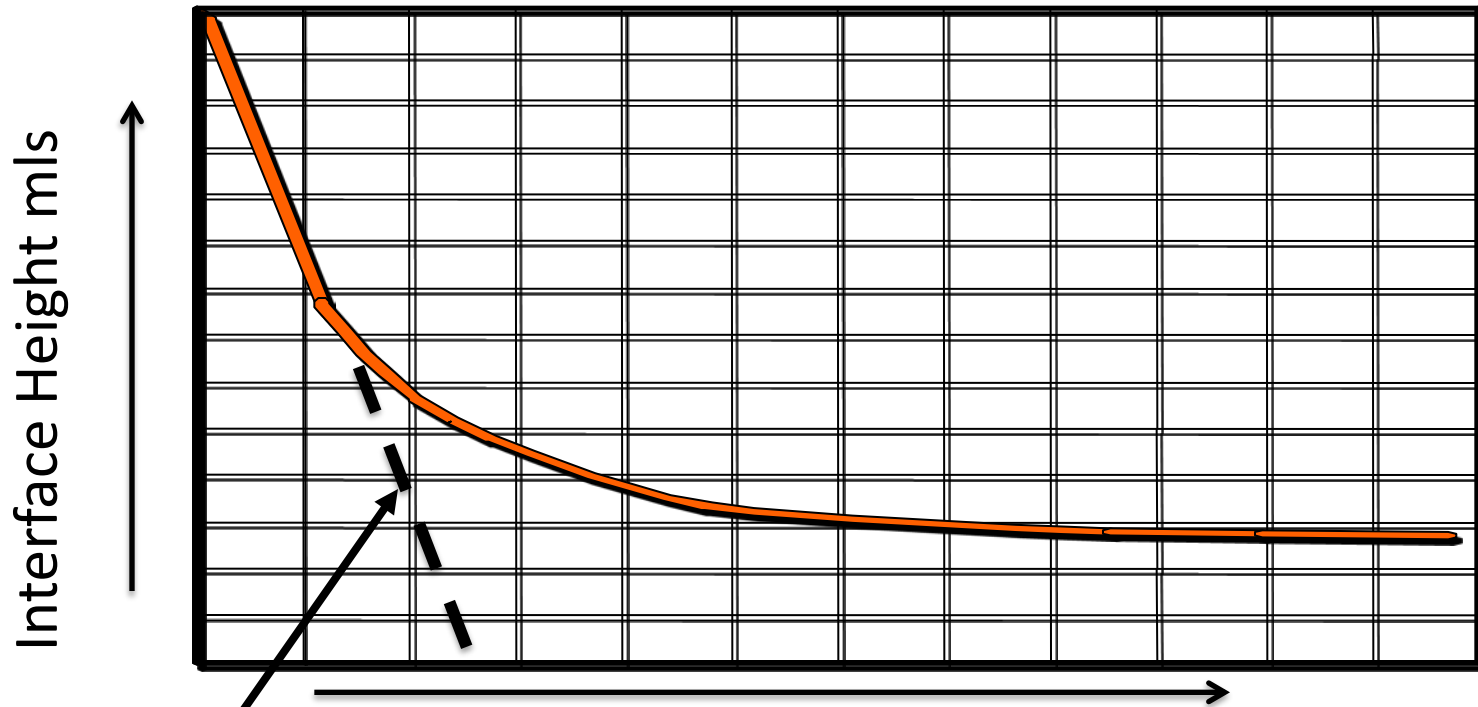
- The upward velocity of effluent in the clarifier/thickener.
- Rise Rate= (Feed Rate-Underflow Rate)/Area

$$\text{Rise Rate} = \frac{\text{m}^3/\text{hr}}{\text{m}^2} = \text{m}/\text{hr}$$



How is Settling Rate Determined?

Interface settling using a graduated cylinder

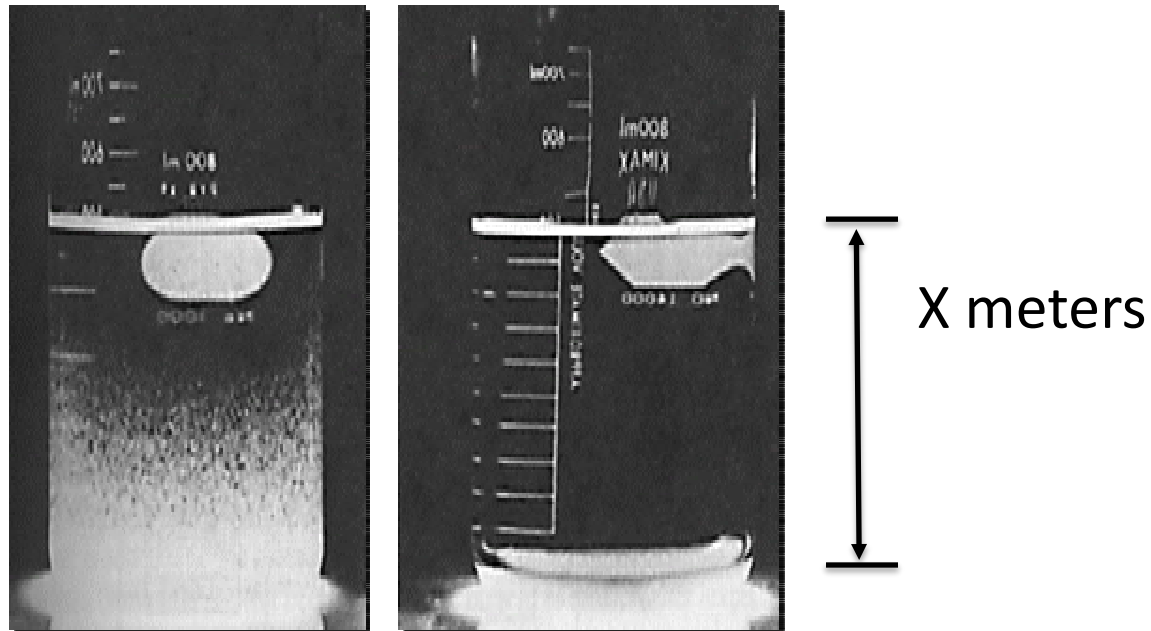


Settling Time Minutes

Slope = Bulk Settling Rate , in m/h or gpm/ft²

How is Settling Rate Determined?

Particulate settling using a beaker and ruler



Bulk Settling Rate = Distance / Time

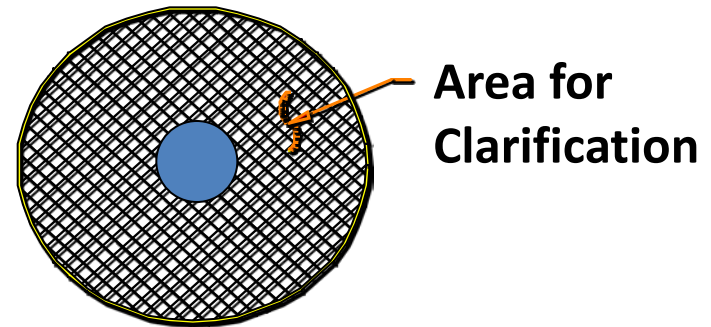
Hydraulic Loading Sizing

$$\text{Settling Rate} * \text{Scale-up Factor} \leq \text{Rise Rate}$$

$$\text{Settling Rate} * 0.5 \leq (\text{Feed Rate} - \text{Underflow Rate}) / \text{Area}$$

Where: Area = surface area of thickener minus feed well area

$$\text{Area} \leq \frac{(\text{Feed Rate} - \text{Underflow Rate})}{\text{Settling Rate} * 0.5}$$

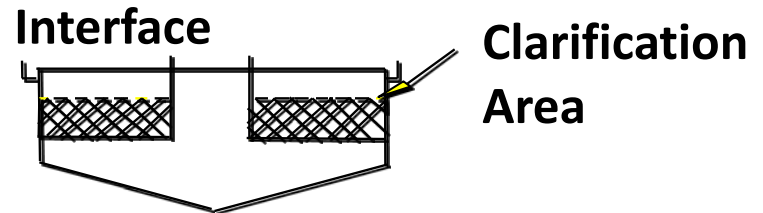


UNITS

$$\text{m}^2 = \frac{\text{m}^3/\text{h}}{\text{m}/\text{h}}$$

or

$$\text{ft}^2 = \frac{\text{gpm}}{\text{gpm}/\text{ft}^2}$$

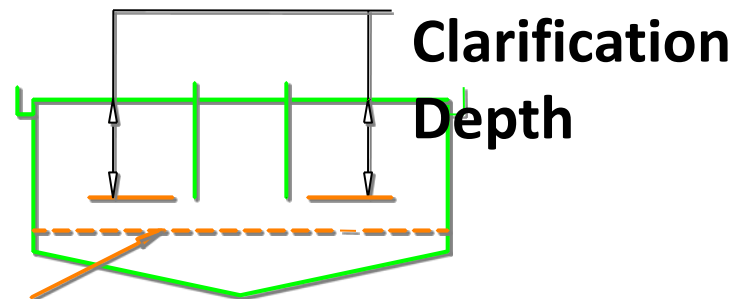
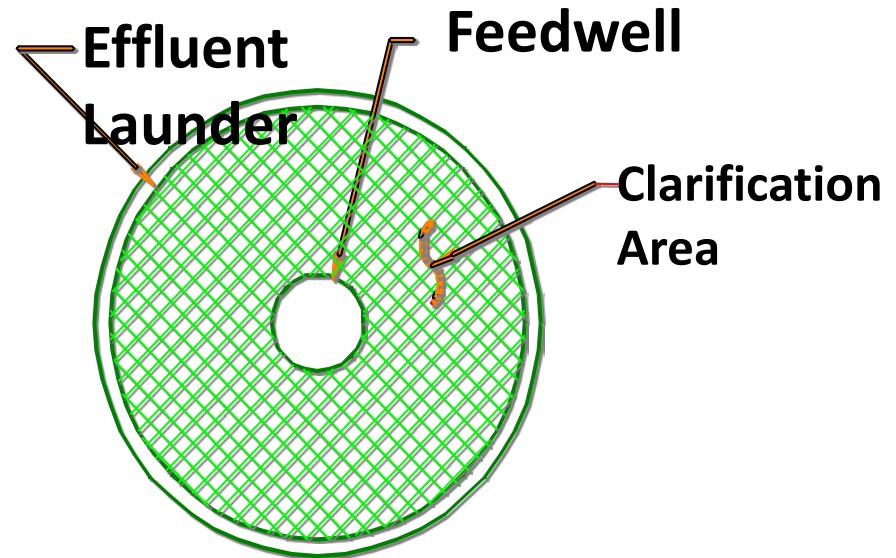


How is the Clarifier Side Wall Height Fixed?

- The minimum side wall height is determined by:
 - Clarification Time
 - An extra long clarification may dictate an increase in diameter

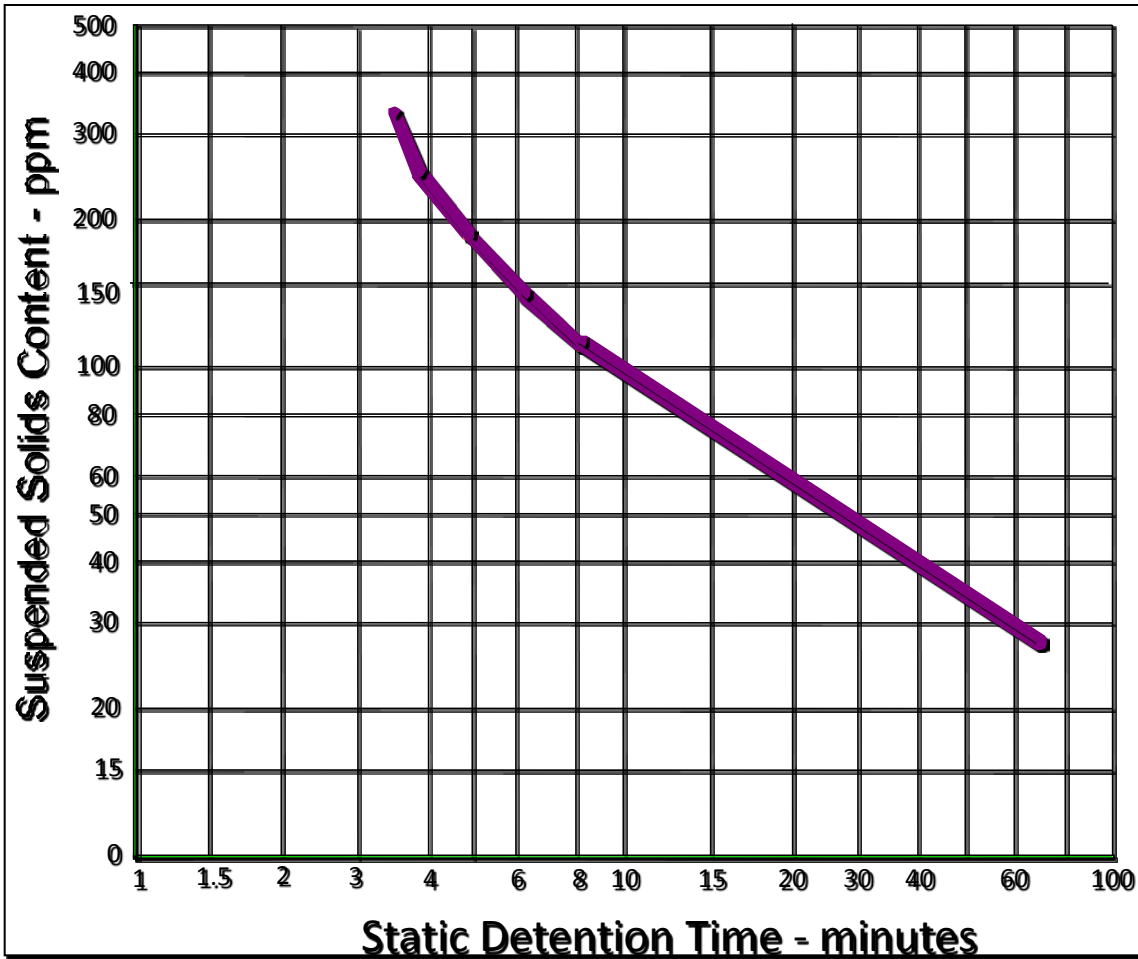
Clarification Time

- Some fine solid or flocs remain in suspension
- In “Time” they agglomerate and settle
- This “Time” is the clarification time
- Observed or “Static” time must be scaled up to operating or “Dynamic” time.



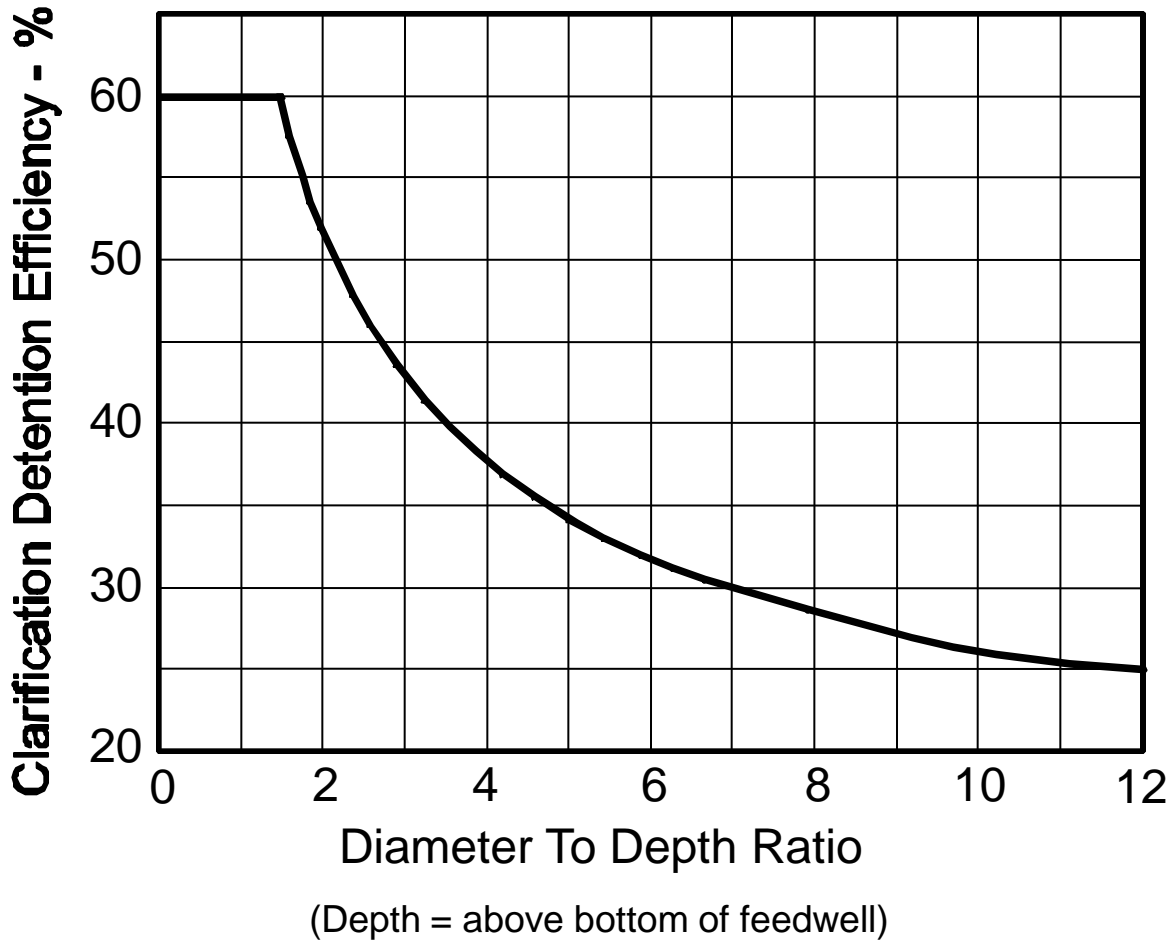
Interface

Determine Clarification Time Flocculated Solids



**Clarification
rate
somewhat
slow, but
typical**

Clarification Detention Efficiency



- An estimate of short-circuiting within tank
- Used to calculate required full scale detention time
- If static detention time = 30 minutes, and dia./depth = 12, nominal detention time = $30/0.25 = 120$ min.
- Use this time to calculate wetted feedwell depth

Feed Solids Limitations

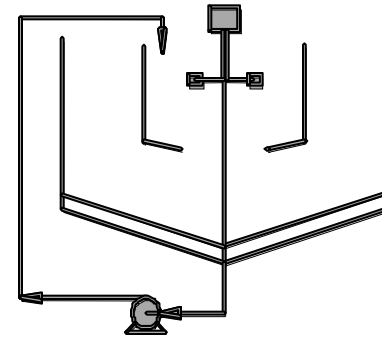
- **Minimum solids required for flocculation**
 - Very dilute suspensions -- difficult / impractical to produce a settleable floc
 - Minimum solids concentration = 300 – 700 mg/L
 - Flocculation improves as solids concentration increases up to a value of at least 0.5 wt.%
 - Upper limit in range of 3.0 wt.% -- At higher concentrations Unit Area may be controlling

Applies to ALL Clarifiers

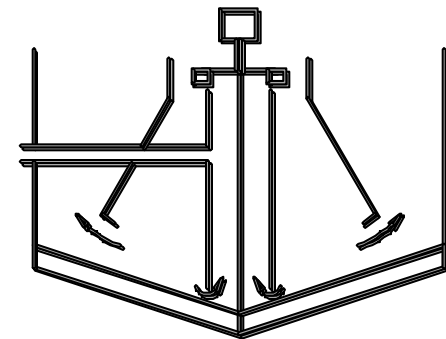
Conventional, Flocculating, Solids Contact

If Solids Concentration Must Be Increased

- Increase solids by external or internal recirculation
- **How to determine?**
 - Bench testing can quickly identify the need for increased solids and the optimum solids concentration



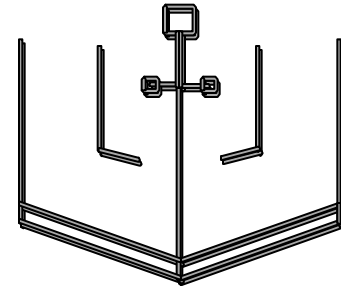
External Recirculation
Underflow Pumping



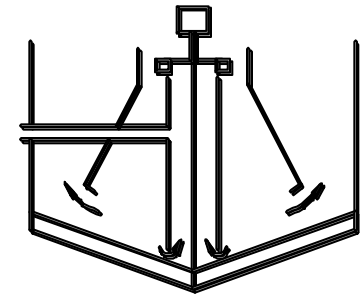
Internal Recirculation
Solids Contact Clarifier
(Draft Tube)

Mechanical Floc Growth

- Flocculation is not always “instantaneous:
 - Gentle mixing and time may be required
 - Liquid phase clears with time
- Observed time to clear must be scaled up to nominal detention time
 - Nominal time = 3 x observed time



Center Flat Blade
Impeller Mixer



Solids Contact
Clarifier

Sludge / Pulp Blanket?

- Purpose:
 - To provide extra liquid/ solids contact time
 - To provide enhanced flocculation of fines
- Consider use:
 - Following a precipitation reaction
 - When high degree of clarity required
- **A blanket is not always possible nor is it necessary for excellent clarity**

Sedimentation

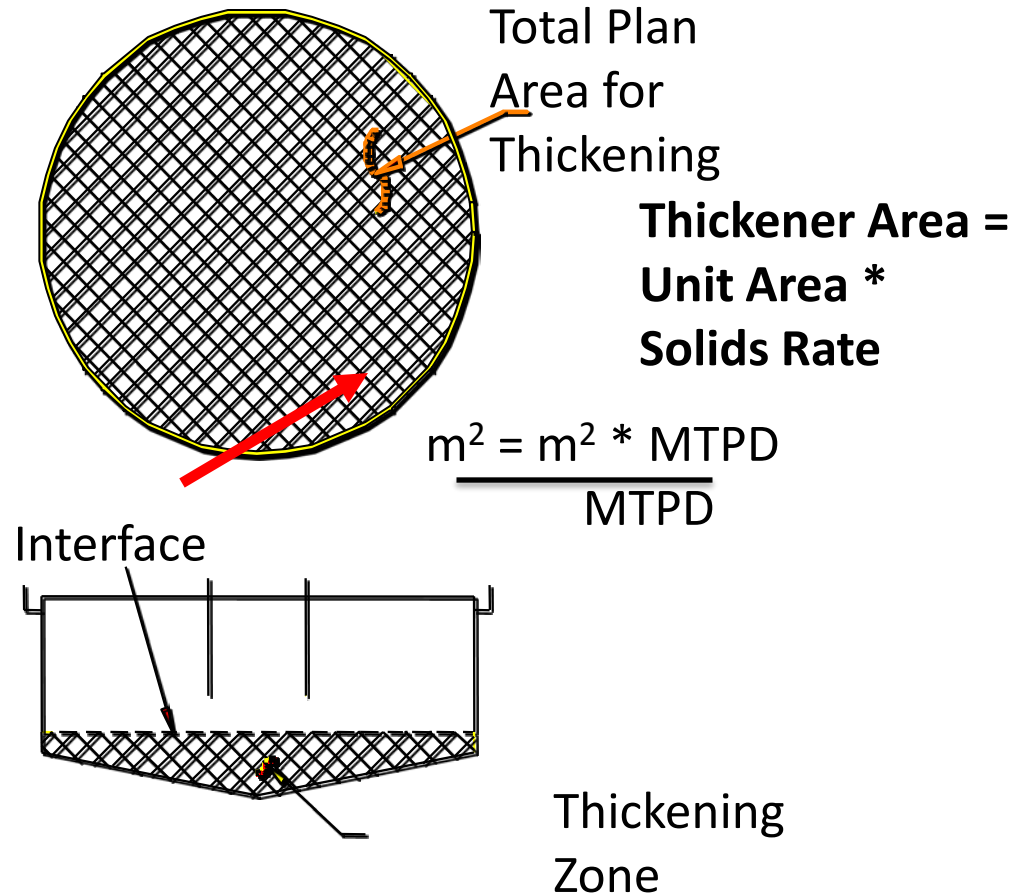
- Thickener Sizing Criteria

How is the Thickener / Clarifier Diameter Fixed?

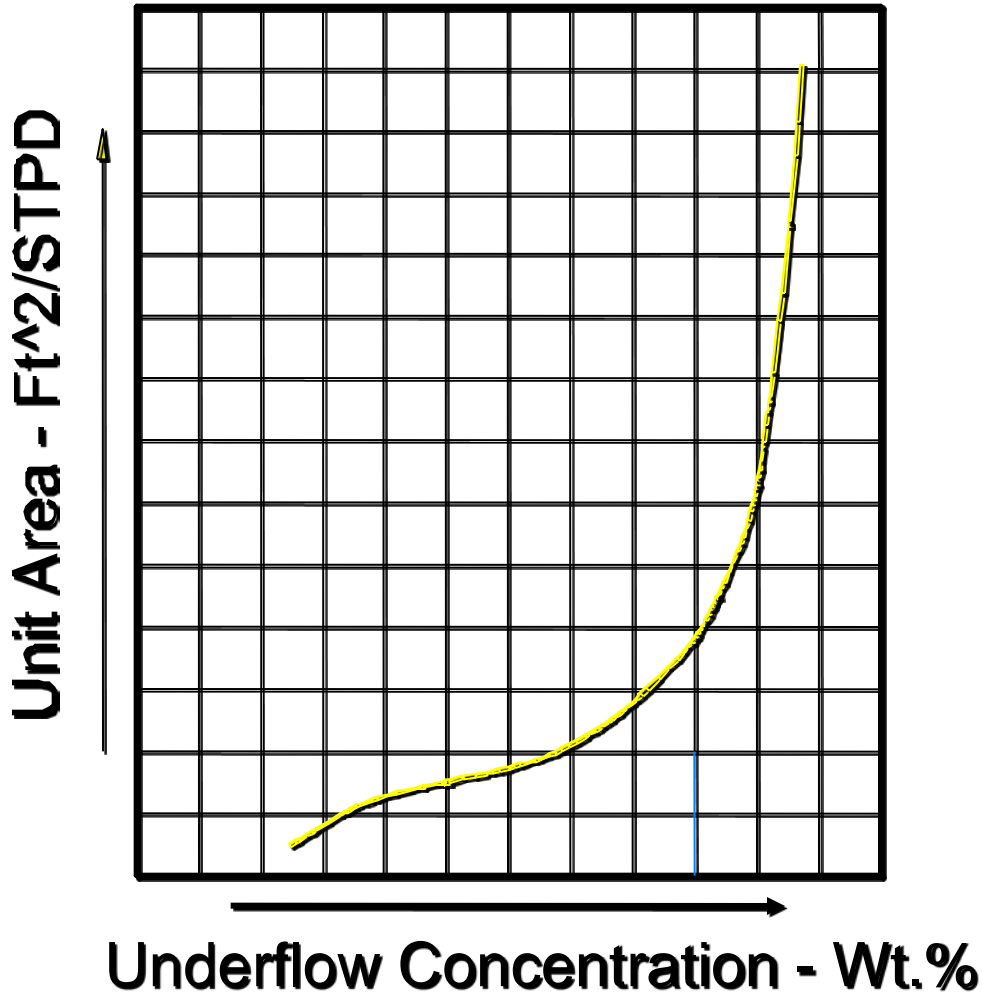
- The minimum diameter is determined by:
 - Settling rate/ rise rate
 - Hydraulic loading
 - Unit Area Requirement
 - Solids loading

Solids Loading - Thickening

- Solids require time to thicken
- Area of thickener provides the time
- Unit Area = area required for a ton per day of solids to thicken to a given concentration



Operating Curve



- Typical curve for conventional thickeners
- Different methods of settling test data interpretation give different results

Sedimentation

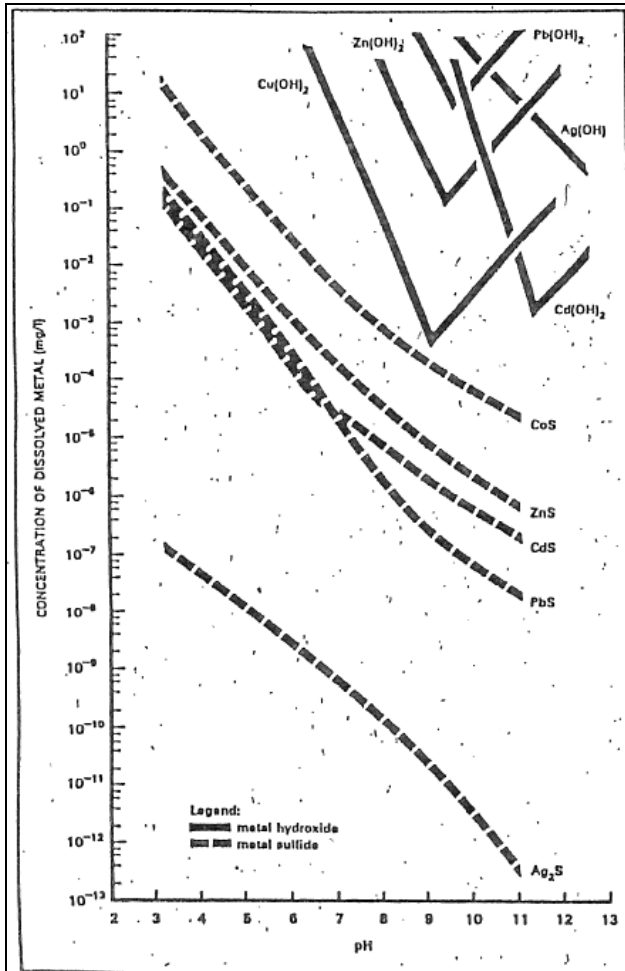
- Flotation
 - Dissolved Air Flotation
 - Induced Air Flotation

Chemical Unit Processes

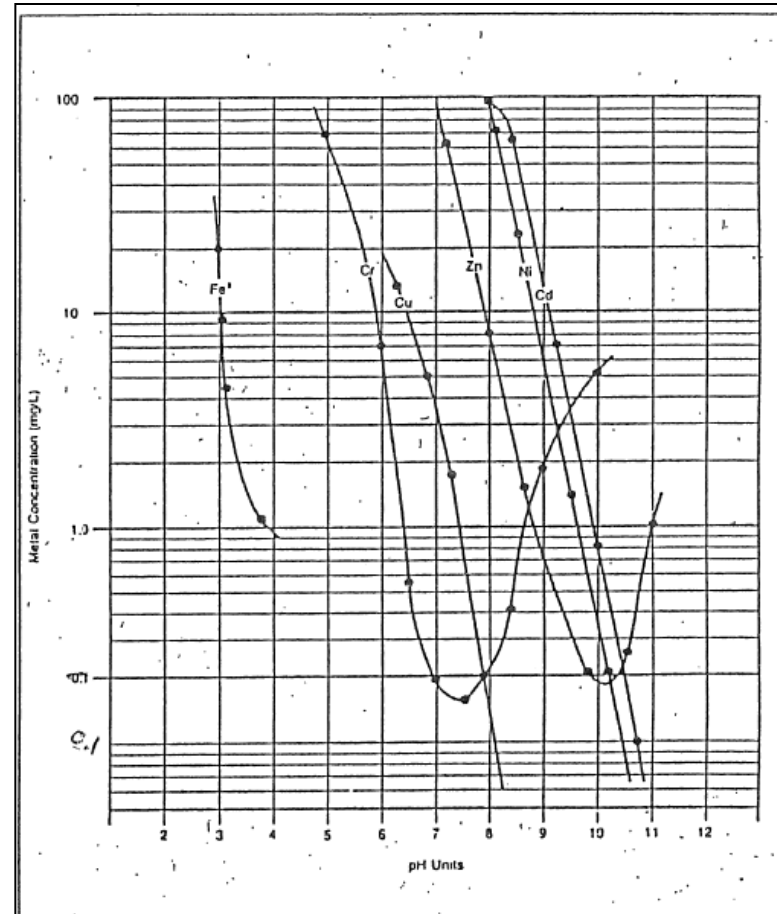
- Precipitation
 - De-supersaturation of Gypsum
 - Cold Lime Softening
 - Metals Removal
 - Metal Hydroxides
 - Metal Sulfides

Solubility of Metals

Metal Sulfide Solubility




Metal Hydroxide Solubility



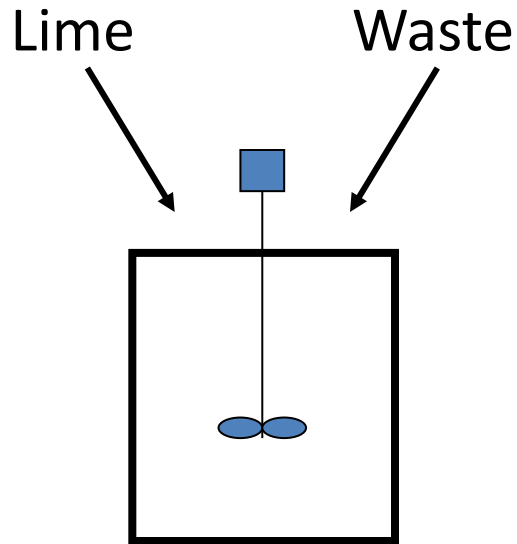
Chemical Unit Processes

- Iron Co-Precipitation
- pH and its effect on solids solubility
- Reactor Design Considerations

Principles of Efficient Precipitation

- Seed the reaction
 - Increase the concentration of previously formed solids in the reaction vessel
 - Mix one of the reactants with previously formed solids before addition of the second reactant
 - Subject formed solids to an elevated pH
 - Provide an extended reaction time
- 

1st Approach To Precipitation

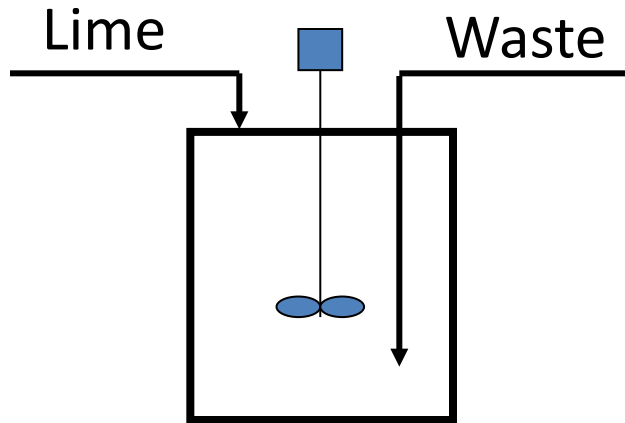


Once Through
Shock Precipitation

Guarantees:

- Maximum number of new particles
- Minimum particle size
- Minimum particle settling rate
- Maximum unit area requirement
- Minimum filtration rate
- Maximum cake moisture content
- Maximum supersaturation

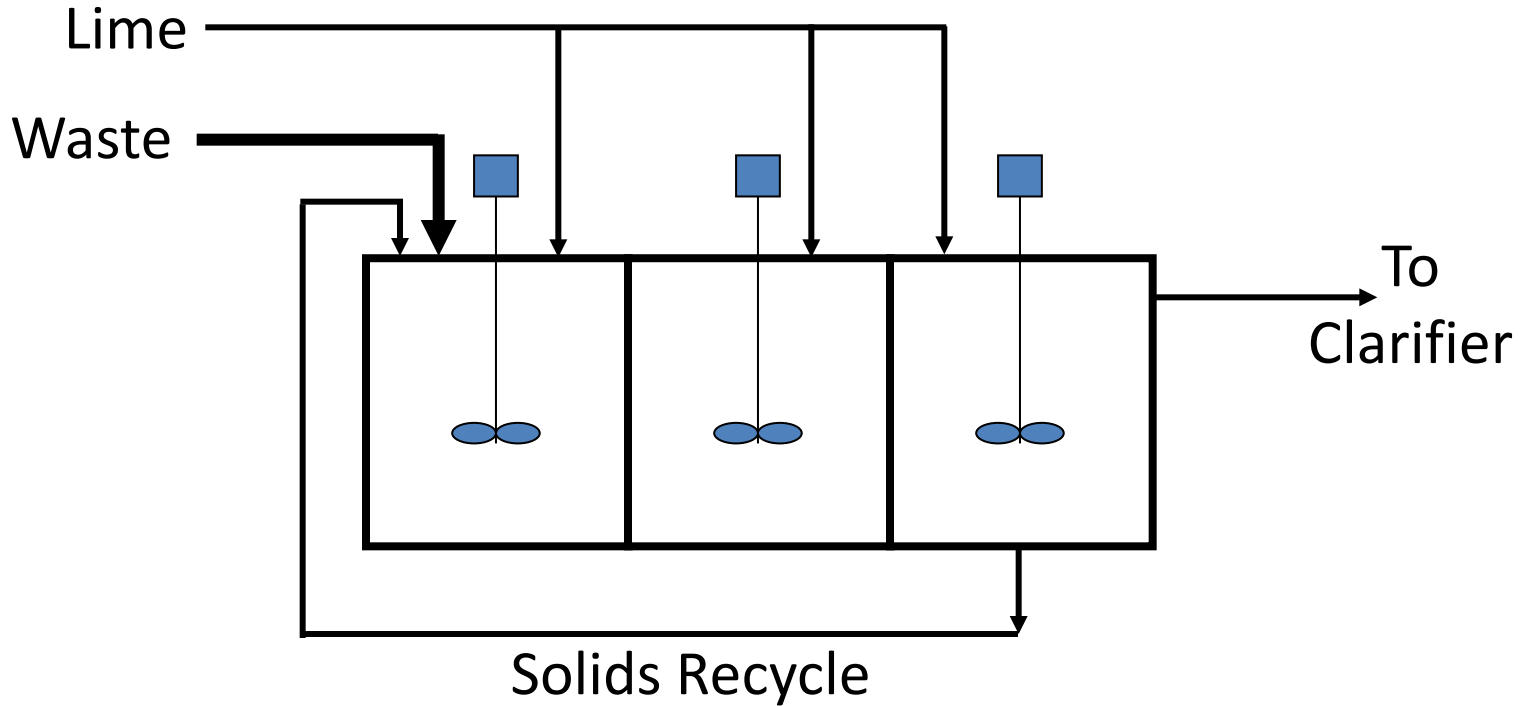
Better Approach To Precipitation



Improves:

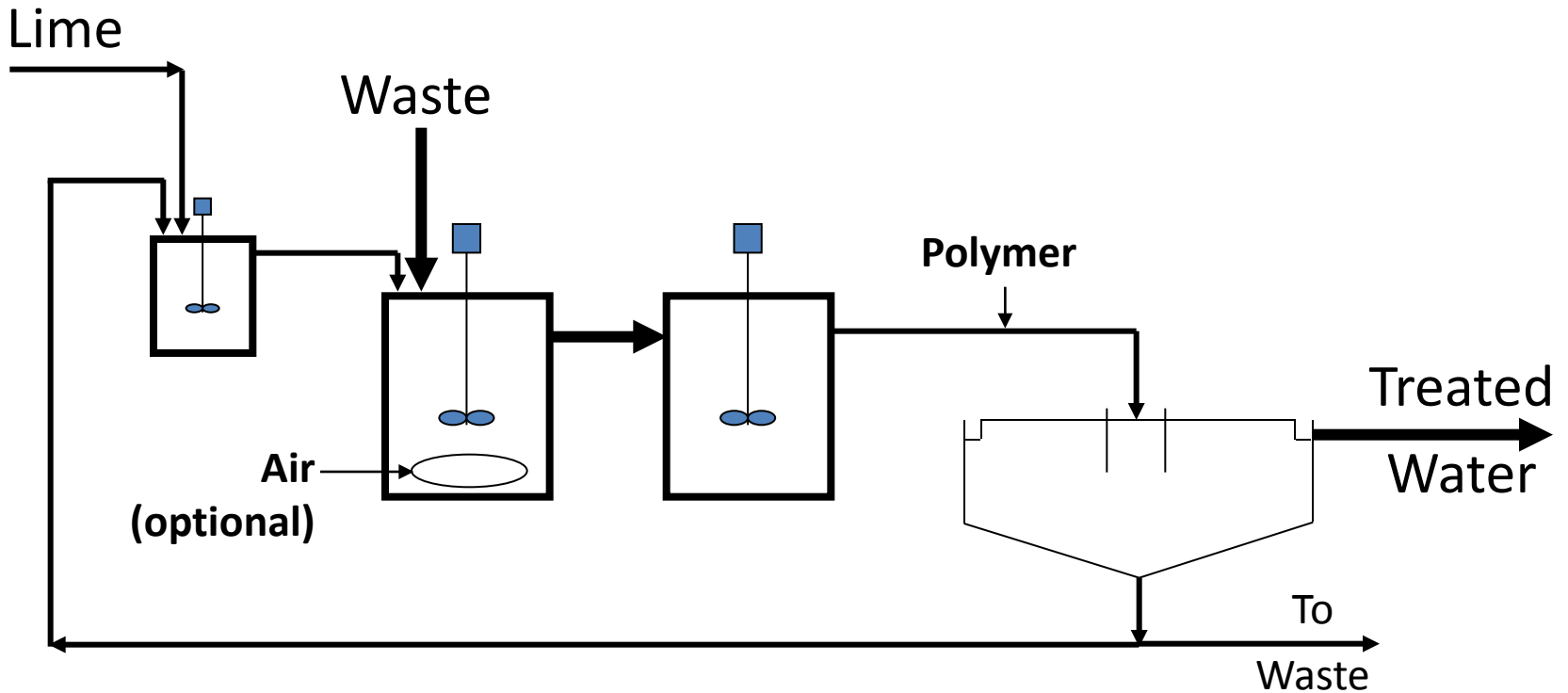
- Particle size
- Desupersaturation
- Scale protection

Better Approach To Precipitation



**This approach starts to experience the
“Advantage Of A Crowd” by John H. Smith, III**

The Basic HDS Flowsheet



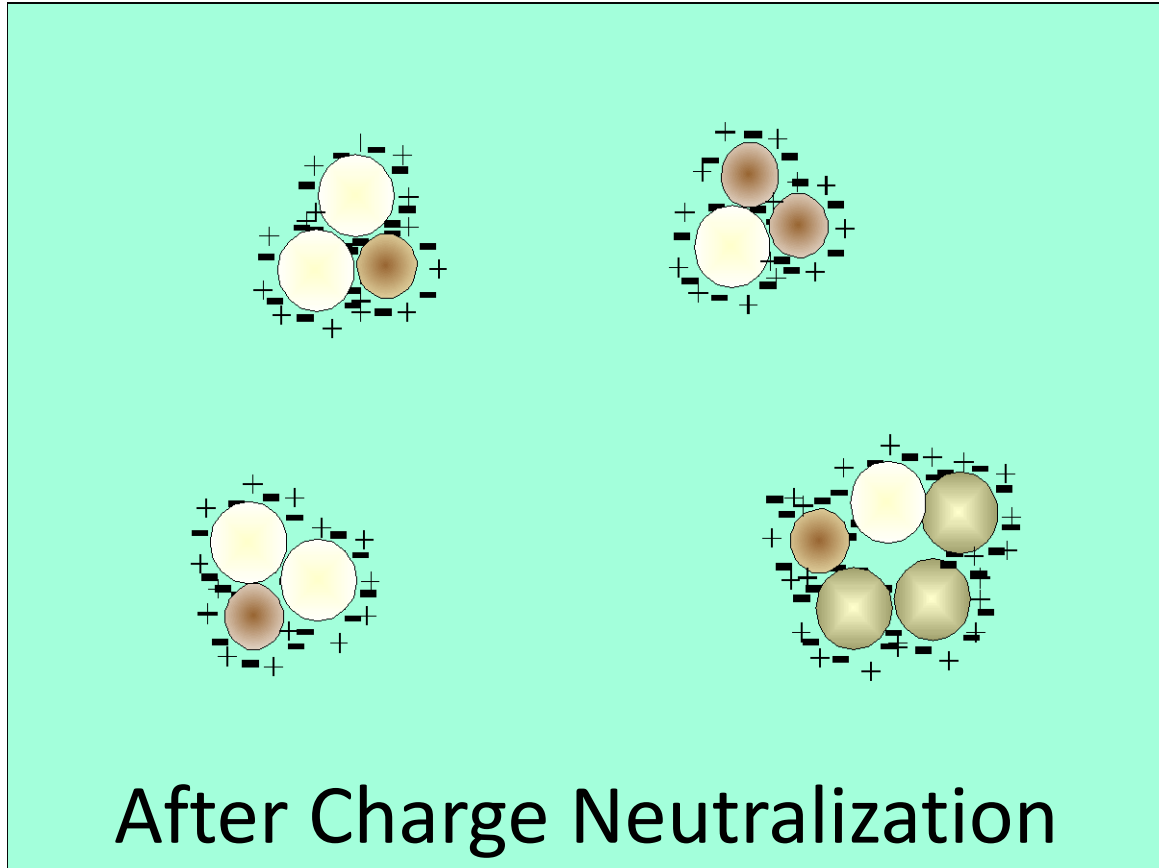
Provides:

- Particle size growth
- Desupersaturation
- Scale protection
- Better lime utilization

Coagulation

- Adding a coagulant to allow agglomeration
 - Coagulants neutralize the negative charge usually associated with naturally occurring particles
 - Usually use cationic multivalent inorganic ions such as Ca^{2+} or Al^{3+}
 - May also be a cationic polymer
 - Flocs form rapidly and reform rapidly after being destroyed by shear

Coagulation After Charge Neutralization



Flocculation

- Anionic
- Nonionic
- Cationic

Flocculation

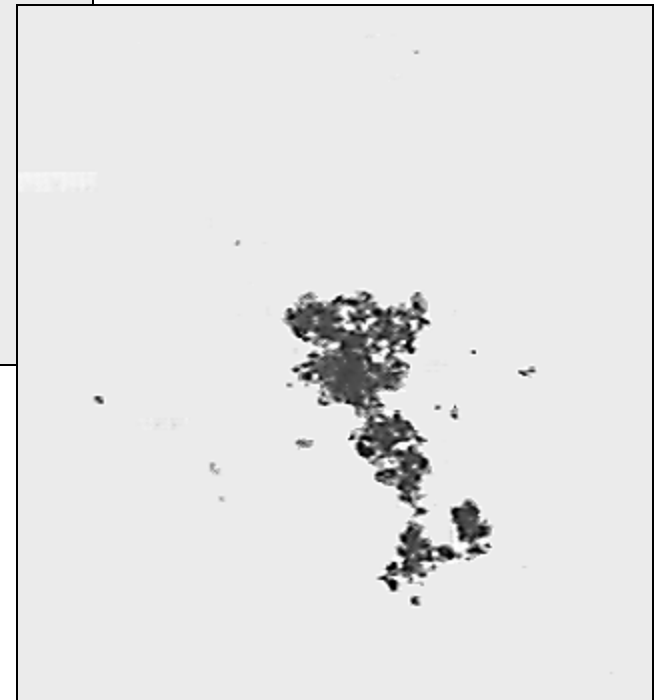
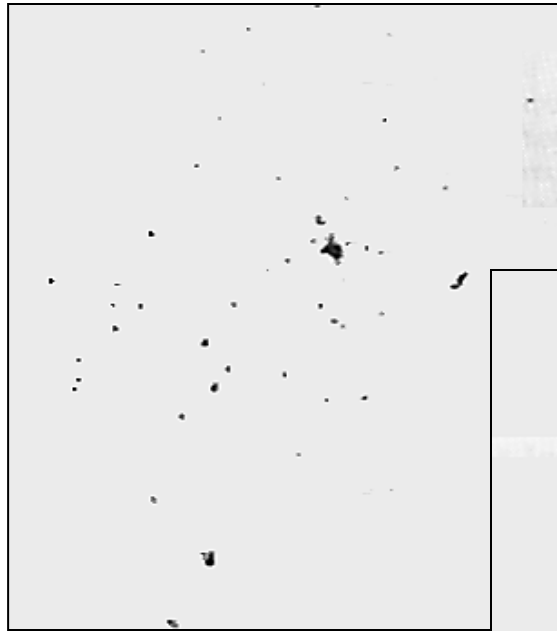
- Adding a long chain polymer
 - May require time for flocs to form
 - Flocs are shear sensitive
 - Never reform as well without the addition of more polymer

NOTE:

- Medium to small flocs are usually best for clarification
- Flocs which settle too rapidly leave fines in suspension

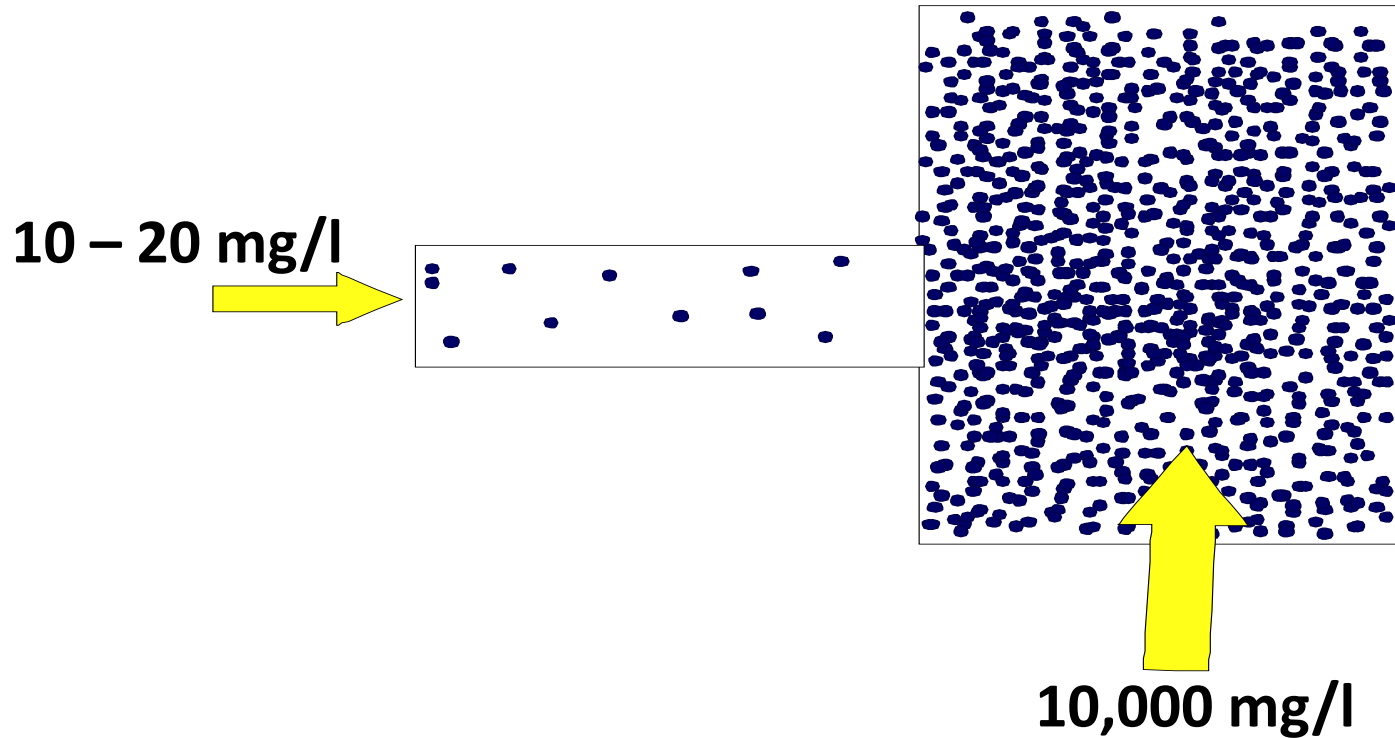
Flocculation

- Little particles into big particles
- Aids both settling rate and clarification

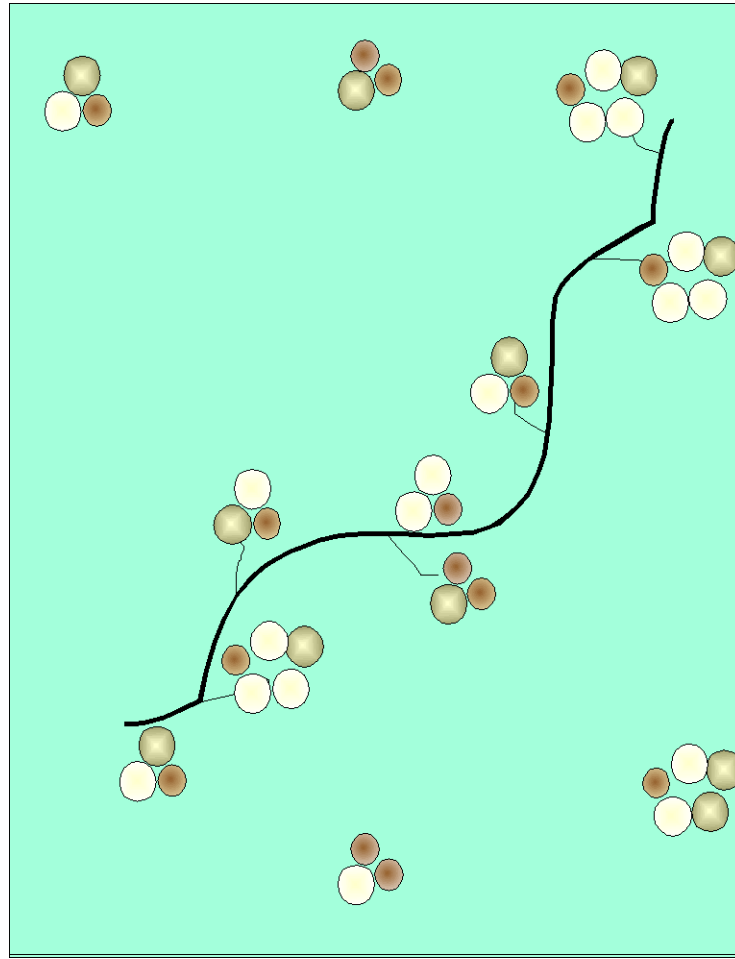


Solids Contact Ratio

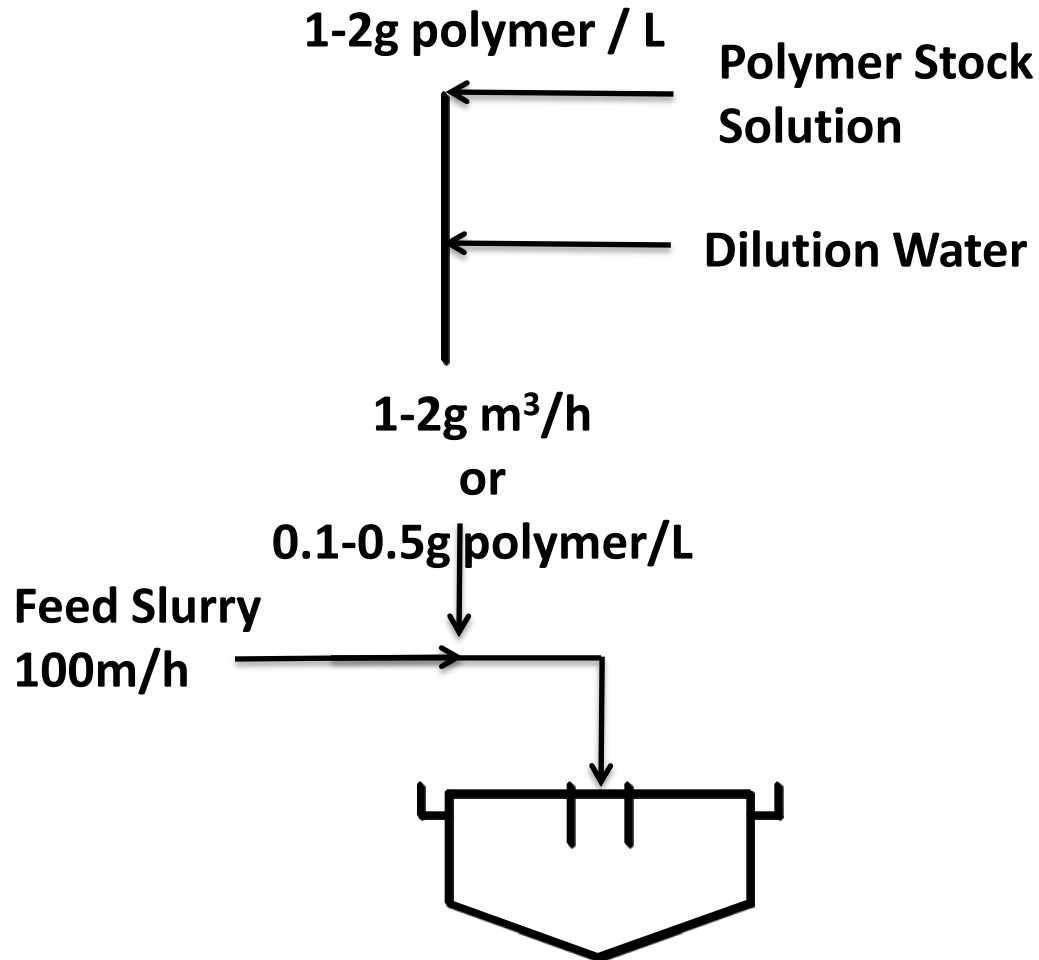
Mass recirculated / Mass in



Flocculation



Polymer Dilution



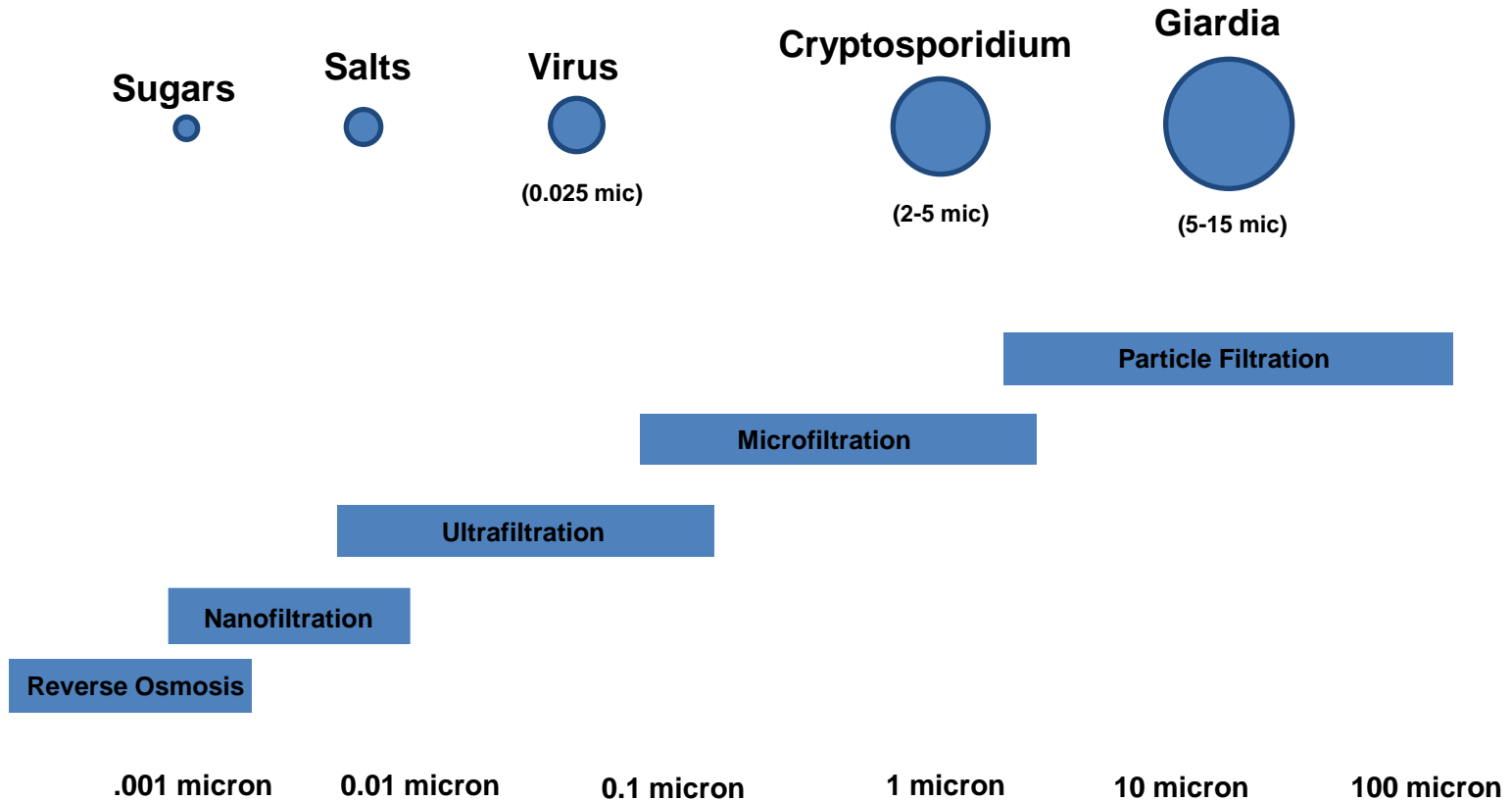
pH Adjustment

- Acid (Hydrochloric vs. Sulfuric)
- Lime (Hydrated vs Quick lime)
- Sodium hydroxide
- Soda ash

Effluent Filtration

- Granular media (super flocculation)
 - Gravity
 - Pressure
- Bag Filtration
- Membrane (barrier)
 - Ultra
 - Nano
 - RO
- Polishing filtration
 - Adsorption media

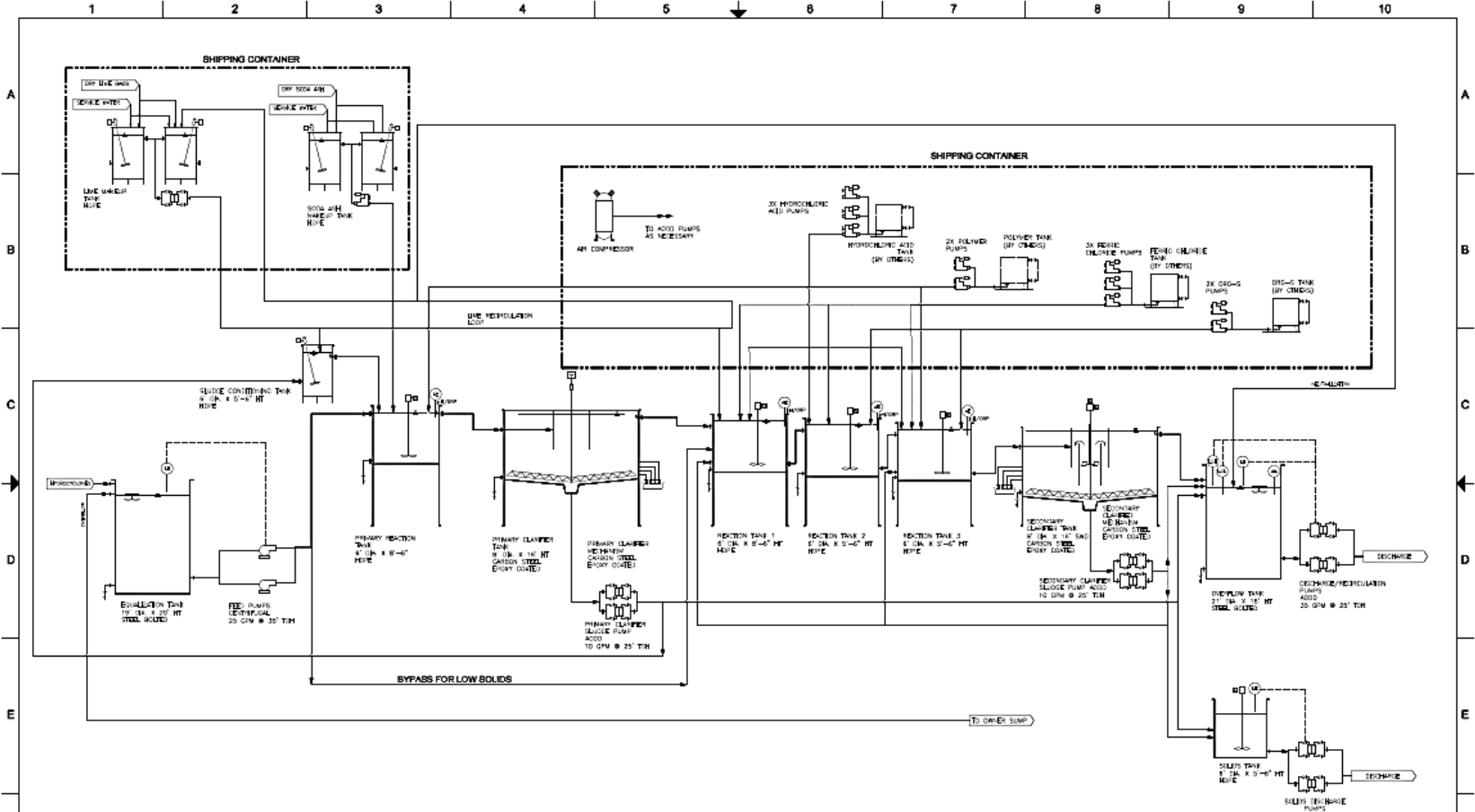
Filtration Spectrum



Solids Dewatering for Disposal

- Equipment options
 - Vacuum Filter
 - Belt Press
 - Plate and Frame Filter Press
 - Centrifuge
- Design for filtrate/pressate return to system
- Design for wash water

Process Flow Diagram



REV	DATE	BY	DATE	DESCRIPTION
1	08/15/03	WJG		INITIAL SUBMITTAL
2	08/20/03	WJG		DESIGN CHECK
3	08/20/03	WJG		DESIGN CHECK
4	08/20/03	WJG		DESIGN CHECK
5	08/20/03	WJG		DESIGN CHECK

PREPARED FOR: SOUTHERN COMPANY SERVICES
 FGD PILOT PLANT
 PLANT MILLER, QUINCY, AL

 ENGINEER: WESTECH ENGINEERING, INC
 SALT LAKE CITY, UT

 CONTRACTOR: MCABEE CONSTRUCTION INC.
 TUSCALOOSA, AL

 PROJECT NUMBER: 90810313794

TITLE: PROCESS FLOW DIAGRAM
 SOUTHERN COMPANY-FGD WW PILOT PLANT

OWNER	DESIGNER	APPROVER	DATE
SCS	WESTECH	WJG	08/15/03
DOCUMENT NUMBER		SHEET	
22663A-PFD01		1 OF 1	
REVISIONS	DATE	BY	REV

Thank you